

IN THE CLAIMS:

1. (Previously Presented) An isocyanate adduct comprising the reaction product of at least one polyisocyanate, having a functionality > 2, with compounds having at least two hydrogen atoms which are reactive toward isocyanate groups, the reaction product providing a polymer matrix that is essentially compact, wherein said adduct has a crystalline content of less than 10 j/g determined by differential scanning calorimetry in accordance with DIN 51 004 at 20 K/min from room temperature to 250°C using a nitrogen flow of 3 l/h as carrier gas and an aromatics content reported as carbon atoms in aromatic rings of less than 31% by weight, based on the total weight of the isocyanate adduct, and wherein the compounds having reactive hydrogen atoms comprise at least one polyetherol bi) having a functionality greater than 3 and a molar mass 300 g/mol or greater.
2. (Previously Presented) An isocyanate adduct as claimed in claim 1 which has a thermal conductivity determined by a hot wire method at 23°C of less than 0.2 W/m*K.
3. (Previously Presented) An isocyanate adduct as claimed in claim 1 further containing fillers.
4. (Previously Presented) An isocyanate adduct as claimed in claim 3, wherein the fillers are hollow microspheres optionally having a pressure loading of greater than 10 bar.
5. (Previously Presented) An isocyanate adduct as claimed in claim 3, wherein the fillers are hollow glass microspheres.
6. (Previously Presented) An isocyanate adduct as claimed in claim 3, wherein the fillers are hollow polymer microspheres.
7. (Previously Presented) An isocyanate adduct as claimed in claim 3, wherein the fillers are hollow ceramic microspheres.
8. (Previously Presented) A process for preparing isocyanate adducts comprising reacting
 - a) isocyanates having a functionality > 2 with
 - b) compounds having at least two reactive hydrogen atoms in the presence of
 - c) catalysts,

wherein the reacting of the components a) and b) provides a polymer matrix that is essentially compact, and

wherein the compounds having reactive hydrogen atoms b) comprise at least one polyetherol bi) having a functionality greater than 3 and a molar mass 300 g/mol or greater, and at least one polyetherol bii) having a molar mass greater than 1000 g/mol and a functionality of from 1.7 to 3 and the reaction is carried out at an index of less than 200.

9. (Previously Presented) A process as claimed in claim 8, wherein the isocyanate a) comprise a mixture of diphenylmethane diisocyanate and polyphenylenopolymethylene polyisocyanates.

10. (Original) A process as claimed in claim 9, wherein the isocyanate is used in an amount of less than 54% by weight, based on the weight of all starting materials.

11. (Original) A process as claimed in claim 10, wherein the component b) further comprises at least one polyetherol biii) having a molar mass of less than 1000 g/mol and a functionality of less than 2.5.

12. (Original) A process as claimed in claim 11, wherein the component b) further comprises at least one polyesterol biv).

13. (Currently Amended) A process as claimed in claim 12, wherein the component b) further comprises at least one bifunctional chain-extender-alcohol bv) having a molecular weight in the range from 62 to 400 g/mol.

14. (Previously Presented) A process as claimed in claim 13, wherein the catalysts used are amine catalysts and/or trimerization catalysts.

15. (Previously Presented) A process as claimed in claim 8, wherein the molar mass of bi) is from 300 to 1000 g/mol.

16. (Previously Presented) An isocyanate adduct as claimed in claim 1 which has a thermal conductivity determined by a hot wire method at 23°C of less than 0.19 W/m*K.

17. (Previously Presented) An isocyanate adduct as claimed in claim 1, wherein the compounds having reactive hydrogen atoms further comprise at least one polyetherol bii) having a molar mass greater than 1000 g/mol and a functionality of from 1.7 to 3.
18. (Previously Presented) An isocyanate adduct as claimed in claim 17, wherein bi) is used in an amount of from 0.1 to 80 parts by weight and bii) is used in an amount of from 0.1 to 99.9 parts by weight, based in each case on the parts by weight of the compounds having reactive hydrogen atoms.
19. (Previously Presented) A process as claimed in claim 8, wherein bi) is used in an amount of from 0.1 to 80 parts by weight and bii) is used in an amount of from 0.1 to 99.9 parts by weight, based in each case on the parts by weight of b).